## Turbulent B.L. cont

SOE3211/2 Fluid Mechanics lecture 6

## 6.1 Skin Friction coefficient (A)

Define a mean skin friction coefficient for an average value of  $\tau_0$ 

$$\overline{C_f} = \frac{\overline{\tau_0}}{\frac{1}{2}\rho U_\infty^2}$$

NB. this is an average over the length of the plate (not a time average!)

Also define a Reynolds number based on the plate length L

$$\mathcal{R}e_L = \frac{U_{\infty}L}{\nu}$$

There are a number of formulae for  $\overline{C_f}(\mathcal{R}e_L)$ 

By integrating the Blasius result

$$C_f = \frac{0.664}{\sqrt{\Re e_x}}, \qquad \overline{C_f} = \frac{1.33}{\sqrt{\Re e_L}}$$

For a turbulent BL. we have the results

$$C_f = \frac{0.0592}{\mathcal{R}e_x^{1/5}}, \qquad \overline{C_f} = \frac{0.074}{\mathcal{R}e_L^{1/5}} \qquad \mathcal{R}e < 10^7$$

Since these are based on empirical data, many different functional relations and constants are around.

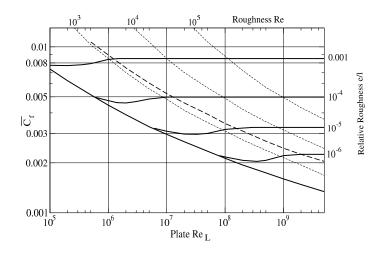
Eg : 
$$\overline{C_f} = 0.455 \left(\log_{10} \mathcal{R} e_L\right)^{-2.58} 10^6 < \mathcal{R} e < 10^9$$

Another important factor determining the skin friction is the roughness

If the peaks of any roughness stick through the BL, this will significantly disrupt flow over the surface – very high friction effect

If on the other hand the peaks are entirely within the laminar sublayer – minimal disruptive effect: the surface is said to be  $hydraulically\ smooth$ 

Skin friction coefficient plotted against  $\mathcal{R}e_L$  for various values of roughness parameter h/L.



## 6.2 Flow around a cylinder

Note – this is a 2-d flow. As  $\mathcal{R}e$  for the flow increases, there are numerous changes in the flow patterns and thus forces on the cylinder. We will start at a low  $\mathcal{R}e$  and work up.

The main force on the cylinder is the drag. Two sources :

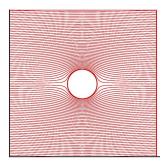
- 1. Pressure distribution around the cylinder Form drag
- 2. Viscous forces in boundary layer Viscous drag/Skin friction drag

Express the drag in terms of a (dimensionless) coefficient  $C_d$ :

$$C_d = \frac{F_d}{\frac{1}{2}\rho A U_0^2}$$

 $C_d$  varies with  $\mathcal{R}e$ :  $C_d = C_d(\mathcal{R}e)$ 

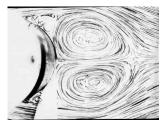
# 6.2.1 Very low $\Re e$ ( $\Re e < 0.5$ )

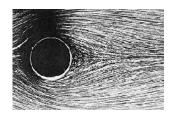


- Flow symmetric front back  $\Rightarrow$  symmetrical pressure distribution around cylinder  $\Rightarrow$  form drag  $\simeq 0$
- Drag forces entirely due to viscosity
- As  $\mathcal{R}e$  increases, flow less symmetric

Note :  $\mathcal{R}e$  are somewhat approximate – depend on roughness of cylinder, details of inlet flow, etc. etc.

### **6.2.2** $2 < \Re e < 30$



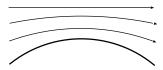


 $(see \ http://www.che.eng.ohio-state.edu/~KOELLING/81508/K_Koelling_81508\_suggestions.htm)$ 

Attached eddies form behind cylinder. Why?

Until now, we have considered *flat* boundary layers with *no* pressure gradient.

Boundary layer on *curved* surface :



Flow must speed up, then slow down (continuity). This implies there must be a pressure gradient along the surface.

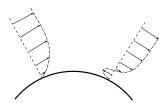
If the pressure decreases in the downstream direction

- the boundary layer reduces in thickness
- $\bullet$  called a favourable pressure gradient

If the pressure *increases* in the downstream direction

- the boundary layer increases in thickness
- $\bullet$  called an *adverse* pressure gradient

If the pressure gradient is sufficiently adverse, it can cause the flow to reverse in the boundary layer. This causes recirculation – the boundary layer is said to separate



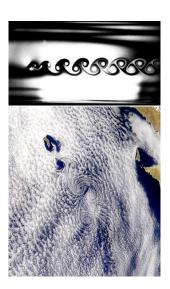
### 6.2.3 von Karman Vortex Street

As  $\Re e$  increases, the trailing vortices lengthen and start to oscillate (30 <  $\Re e$  < 90).

Eventually they fall off and are carried downstream (250  $< Re < 10^3$ ).

- the von Karman Vortex street

(see Nasa web site)



The vortices are shed from alternate sides of the cylinder. As one is shed, a new one grows on the other side. Thus, downstream is a double row of vortices being carried along in the flow

- 2 facts about vorticity:
- 1. In many flows vorticity is conserved
- 2. A body with associated vorticity in a flow experiences a transverse (lift) force the Magnus effect

We will discuss the Magnus effect later (wings, aerofoils).

If the cylinder sheds a (+) vortex, it retains an opposite vorticity (-) attached – thus it experiences a force in one direction.

When the opposite vortex is shed, it carries off the (-) vorticity – the cylinder now has (+) vorticity, so experiences a force the other way.

Thus the cylinder will (try to) vibrate – Aeolean harp effect

#### Examples

- Singing pylons
- Unlaiden roofracks
- Tacoma narrows bridge

Look at the following:

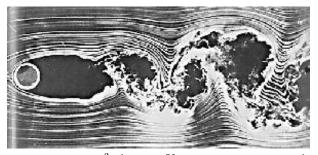
- Nasa web site http://daac.gsfc.nasa.gov/oceancolor/scifocus/oceanColor/vonKarman\_vortices.shtml includes an animation of vortex shedding
- $\bullet \ \ {\rm Tacoma\ Narrows\ bridge\ disaster\ http://www.enm.bris.ac.uk/research/nonlinear/tacoma/tacoma.html}$

We can define a dimensionless number for this – the Strouhal number. If the frequency of vibration is f then

$$Str = \frac{fd}{U_0} = 0.198 \left( 1 - \frac{19.7}{\mathcal{R}e} \right)$$

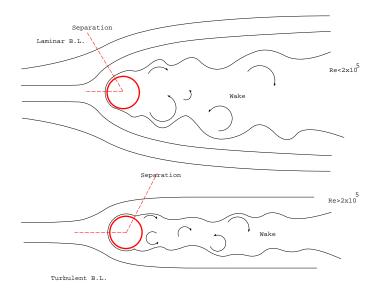
(valid for  $250 < \mathcal{R}e < 2 \times 10^5$ )

### 6.2.4 Turbulent wake region

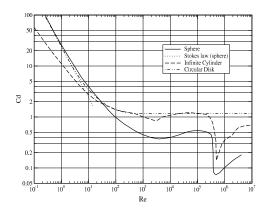


For  $\Re e > 10^3$  the von Karman vortex street degenerates into a turbulent wake. The boundary layer in front is still laminar, but separates at an angle of 81°

At  $\mathcal{R}e \sim 5 \times 10^5$  the boundary layer becomes turbulent. This delays separation, (which now occurs behind the cylinder rather than in front) leading to a reduced form drag. This drop in drag is known as the *drag crisis*.  $F_d$  as well as  $C_d$  can be reduced by increasing  $U_0$  in this region.



We can plot  $C_d(\mathcal{R}e)$  for cylinders over this range of flow conditions:



#### To summarise:

- $\Re e < 0.5$ : no separation, low form drag, symmetrical.  $C_d$  varies as  $U_0$  because of the skin friction drag (drag proportional to  $U_0$ ).
- $2 < \mathcal{R}e < 30$ : separation occurs, attached eddies. Significant form drag because symmetry broken.  $C_d$  varies as  $U_0^2$  since the point of separation shifts.
- $30 < \Re e < 90$ : attached eddies become unstable
- $250 < \mathcal{R}e < 10^3$ : von Karman vortex street.
- $10^3 < \mathcal{R}e < 5 \times 10^5$ : laminar boundary layer up to 81°, then separation. Pressure drag  $\gg$  skin friction; drag coefficient pretty constant.

•  $\Re e > 5 \times 10^5$ : boundary layer becomes turbulent. Separation delayed, so lower pressure drag, drag crisis.

#### Some other websites

- Dantec dynamics http://www.dantecdynamics.com/Education/Animations/Index.html
- Virtual Album of Fluid Motionhttp://www.featflow.de/album/index.html
- Some CFD-generated results.http://www.lstm.uni-erlangen.de/~breuer/
- $\bullet \ \ Pictures \ of \ cylinders \ in \ laminar \ flow \ http://www.media.mit.edu/physics/pedagogy/nmm/student/95/ariedynamics.$
- $\bullet \ \ Some further \ examples \ http://enstrophy.colorado.edu/~mohseni/FluidInstabilityPictures1.html$